

RAPID COMMUNICATION

## Electrochemical synthesis of ammonia from water and nitrogen catalyzed by nano- $\text{Fe}_2\text{O}_3$ and $\text{CoFe}_2\text{O}_4$ suspended in a molten $\text{LiCl-KCl-CsCl}$ electrolyte

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(Received 28 December 2015 • accepted 19 March 2016)

**Abstract**—Nano- $\text{Fe}_2\text{O}_3$  and  $\text{CoFe}_2\text{O}_4$  were suspended in molten salt of alkali-metal chloride ( $\text{LiCl-KCl-CsCl}$ ) and their catalytic activity in electrochemical ammonia synthesis was evaluated from potentiostatic electrolysis at 600 K. The presence of nanoparticle suspension in the molten chloride resulted in improved production of  $\text{NH}_3$ , recording  $\text{NH}_3$  synthesis rate of  $1.78 \times 10^{-10} \text{ mol s}^{-1} \text{ cm}^{-2}$  and  $3.00 \times 10^{-10} \text{ mol s}^{-1} \text{ cm}^{-2}$  with  $\text{CoFe}_2\text{O}_4$  and  $\text{Fe}_2\text{O}_3$ , which are 102% and 240% higher than that without the use of a nanocatalyst, respectively. We speculated that the nanoparticles triggered both the electrochemical reduction of nitrogen and also chemical reaction between nitrogen and hydrogen that was produced from water electro-reduction on cathode. The use of nanocatalysts in the form of suspension offers an effective way to overcome the sluggish nature of nitrogen reduction in the molten chloride electrolyte.

Keywords: Ammonia, Electrochemical Reduction, Molten Salt, Nano-catalysts

### INTRODUCTION

Ammonia ( $\text{NH}_3$ ) is an important fertilizer and nitrogen precursor. This essential substance, currently the second most produced chemical on this planet [1], has also been regarded as a green energy carrier; when compared to the conventional energy carrier, hydrogen, storage and transportation are far cheaper and easier [1]. Its production is primarily done by a process termed the Haber-Bosch (H.B.) process, which converts more than 120 million tons of nitrogen ( $\text{N}_2$ ) to  $\text{NH}_3$  every year [2]. This old and mature technology, however, is energy-intensive *per se*: very high temperature (~500 °C) and pressure (~200 bar) are required even in the presence of potent catalysts, resulting in the consumption of over 30 GJ per ton of  $\text{NH}_3$  produced [3-5]. Besides, one of reactants hydrogen is prepared via the steam reforming of natural gas, and as a result a massive amount of  $\text{CO}_2$  is emitted: 1.87 ton  $\text{CO}_2$  is released per ton of  $\text{NH}_3$  produced [6], suggesting the product is not at all a green carrier after all. Accordingly, it is of great importance to develop an alternative with the nature of true sustainability.

Electrochemical  $\text{NH}_3$  synthesis is one such candidate: it is estimated to be able to reduce the total energy consumption (over 20% compared to the H.B. process) and yet allows to avoid immediate carbon emission [1,6]. If electricity is provided from renewable sources especially on a commercial scale, in particular, this electrochemical way has a great potential to position  $\text{NH}_3$  to act as a workable green energy carrier [6].

Among electrochemical platforms explored thus far, molten alkali-metal chloride (i.e.,  $\text{LiCl-KCl-CsCl}$ -based electrolyte has drawn

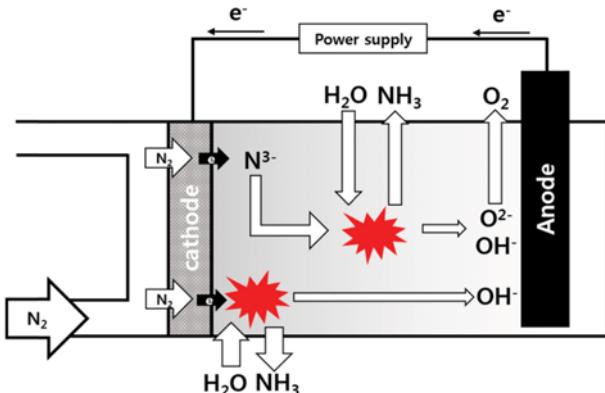


Fig. 1. The principle of electrochemical synthesis of  $\text{NH}_3$  from water and  $\text{N}_2$  in  $\text{LiCl-KCl-CsCl}$  molten salt (Ref. [8]). Reactions that are likely to happen are stated.

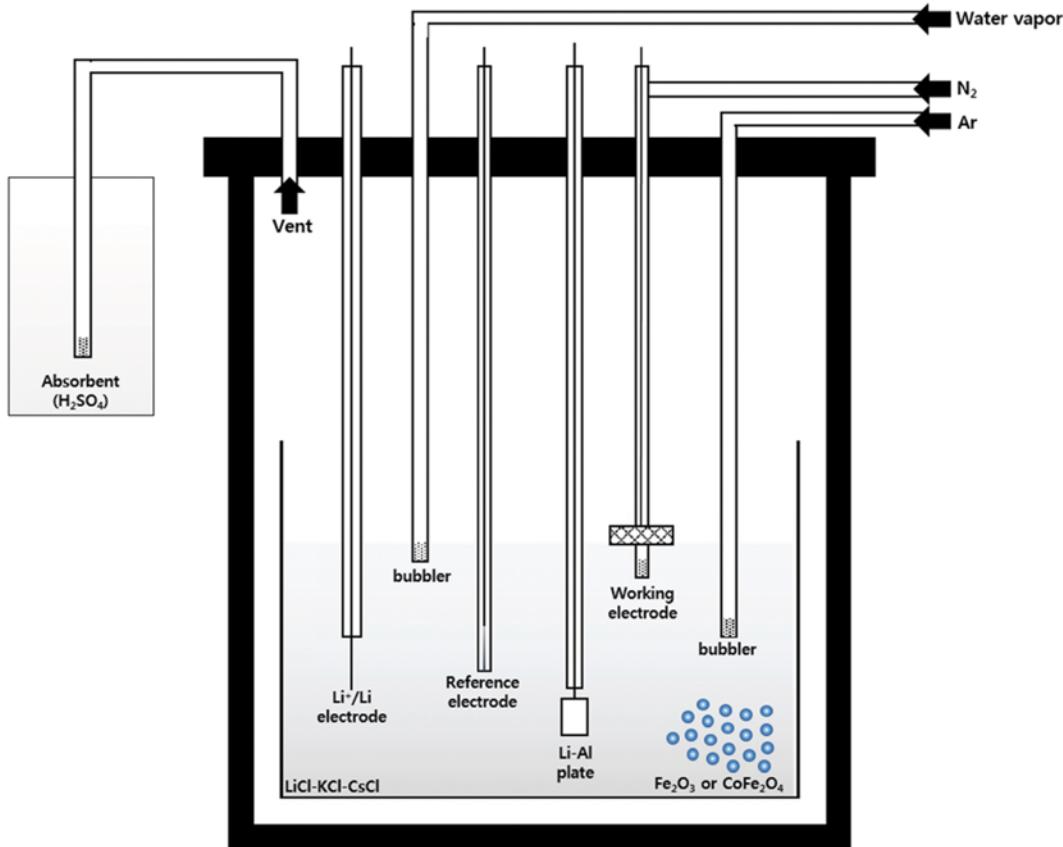
continuous attention owing to its high ionic conductivity, thermodynamic stability, wide electrochemical window, and low vapor pressure [7,8]. Using this electrolyte, Murakami and others investigated  $\text{NH}_3$  synthesis from  $\text{N}_2$  and various hydrogen sources (H<sub>2</sub>, H<sub>2</sub>O, CH<sub>4</sub>, H<sub>2</sub>S, and HCl) at ambient pressure, and the underlying principles are rather well stated in the previous publications as well as in Fig. 1 [9-14]. This molten chloride-based  $\text{NH}_3$  electro-synthesis, however, is still far from being commercially viable. One critical barrier is the sluggish reduction of  $\text{N}_2$  due to the extremely strong triple bond between N atoms (941 kJ mol<sup>-1</sup>) [6,15]. Our aim, therefore, was to speed up this rate-limited step, especially by including mediators in the form of nanoparticles suspended in the molten liquid electrolyte.

Licht et al. attempted to use iron oxide ( $\text{Fe}_2\text{O}_3$ ) nanoparticles as a suspended catalyst for  $\text{NH}_3$  synthesis in their molten hydroxide

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**Fig. 2.** A schematic representation of experimental apparatus.

electrolyte (NaOH-KOH) [2], and in an ensuing study, detailed mechanisms were speculated [16]. In this study, CoFe<sub>2</sub>O<sub>4</sub> as well as Fe<sub>2</sub>O<sub>3</sub> nanoparticles were suspended in the molten LiCl-KCl-CsCl electrolyte and employed as nanocatalysts for electrochemical NH<sub>3</sub> synthesis.

## MATERIALS AND METHODS

Fig. 2 shows a schematic illustration of the experimental apparatus. All experiments were carried out in argon (Ar) only atmosphere [17]. Reagent grade LiCl, KCl, and CsCl were purchased from Sigma Aldrich. Their mixture (LiCl:KCl:CsCl=57.5:13.3:29.2 mol%, [9-14]) was prepared in an Ar-filled glove box and then dried under vacuum at least for 24 h at 373 K to remove moisture. The eutectic mixture was melted at around 600 K in a furnace, followed by a treatment with diluted HCl gas (HCl : Ar=1:99) for 8 h to prevent hydrolytic decomposition of molten chloride [18]. The temperature was kept at 600 K throughout the experiment. The working electrode, which acted to reduce N<sub>2</sub>, consisted of porous Ni ( $\varnothing 4.5\text{ cm} \times 1\text{ cm}$ , specific surface area:  $1,000\text{ m}^2\text{ m}^{-3}$ ). Before NH<sub>3</sub> synthesis, 0.3 V (vs. Li<sup>+</sup>/Li) was applied on the working electrode overnight to reduce oxide films on its surface. The counter electrode was Li-Al alloy in the ( $\alpha+\beta$ ) coexisting phase state [9,19]. Ag<sup>+</sup>/Ag was used as the reference electrode in another LiCl-KCl-CsCl eutectic melt. All potentials in this study were referenced to an Li<sup>+</sup>/Li electrode.

Fe<sub>2</sub>O<sub>3</sub> (Sigma Aldrich,  $A_{BET}: 35.42\text{ m}^2\text{ g}^{-1}$ ) and CoFe<sub>2</sub>O<sub>4</sub> (Sigma Aldrich,  $A_{BET}: 57.14\text{ m}^2\text{ g}^{-1}$ ), used as nanocatalysts in this study, were suspended in the molten salt. Considering  $A_{BET}$  values, an appropriate amount of each nanocatalyst was added to the melt so that the two catalysts had the same total area of  $285.7\text{ m}^2$ .

Potentiostatic electrolysis, with and without each nanocatalyst, was carried performed for 2 h by applying 0.2 V on the working electrode, which was fed with N<sub>2</sub> with a flow rate of 200 sccm. At the same time, water vapor was provided to the melt by flowing 50 sccm of Ar, which passed through a bath of distilled water at 303 K. The vent gas from the reactor was collected in dilute sulfuric acid (0.001 M), and NH<sup>4+</sup> concentration in the absorbent was determined with an ammonia meter (Palintest 1000, Nessler's method). The current efficiency for synthesized NH<sub>3</sub> was defined as the charge used for NH<sub>3</sub> synthesis divided by total charge passed through the electrolytic cell.

## RESULTS AND DISCUSSION

Potentiostatic electrolysis was done for 2 h, with and without each nano-catalyst, by applying 0.2 V on the working electrode. This potential level was expected to ensure a reducing environment enough to form nitride (N<sup>3-</sup>) [15,20], a highly reduced monoatomic anion that instantaneously and spontaneously reacts with water to form NH<sub>3</sub> [10,11]. The current densities at plateau during the electrolysis were - 13 mA cm<sup>-2</sup>, - 17 mA cm<sup>-2</sup>, and - 22 mA cm<sup>-2</sup>

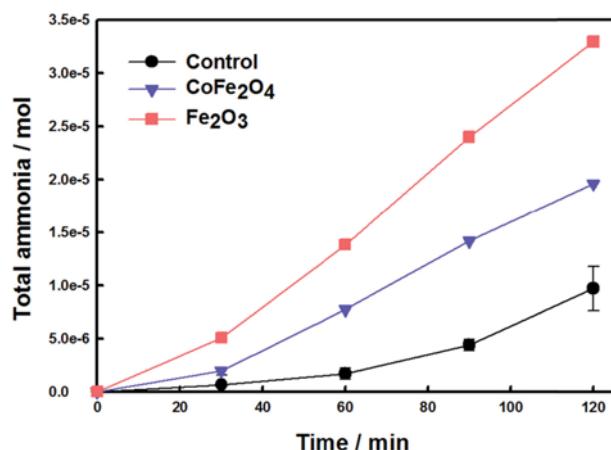


Fig. 3. Cumulative production of  $\text{NH}_3$  for 2 h during potentiostatic electrolysis with and without nano-catalysts suspended in the molten salt (working electrode potential: 0.2 V vs.  $\text{Li}^+/\text{Li}$ ,  $\text{N}_2$  flow rate: 200 sccm, temperature: 600 K).

for control (no nano-catalyst),  $\text{CoFe}_2\text{O}_4$ , and  $\text{Fe}_2\text{O}_3$ , respectively. The increase in the overall current density in the presence of nano-catalysts was attributable partially to marginal yet discernible dendritic deposition of Fe or Co on the working electrode [21-23]. In addition, enhanced electrochemical  $\text{N}_2$  reduction catalyzed by nano-catalysts seemed to be another important cause of the increase, as discussed later.

Fig. 3 shows cumulative  $\text{NH}_3$  production during the potentiostatic electrolysis with and without nanocatalysts. Clearly, the presence of nano-catalysts did enhance  $\text{NH}_3$  synthesis all the time; and  $\text{Fe}_2\text{O}_3$  was more active than  $\text{CoFe}_2\text{O}_4$ . The total  $\text{NH}_3$  production for 2 h was  $9.71 \times 10^{-6}$  mol,  $1.96 \times 10^{-5}$  mol, and  $3.30 \times 10^{-5}$  mol for control,  $\text{CoFe}_2\text{O}_4$ , and  $\text{Fe}_2\text{O}_3$ , which corresponded to  $\text{NH}_3$  synthesis rates of  $8.83 \times 10^{-11}$  mol  $\text{s}^{-1}$   $\text{cm}^{-2}$ ,  $1.78 \times 10^{-10}$  mol  $\text{s}^{-1}$   $\text{cm}^{-2}$ , and  $3.00 \times 10^{-10}$  mol  $\text{s}^{-1}$   $\text{cm}^{-2}$ , respectively. This  $\text{NH}_3$  yield in the order of  $\text{Fe}_2\text{O}_3 > \text{CoFe}_2\text{O}_4 >$ control accorded with the trend in the magnitude of the current densities. This suggested that the increase in current density, which in turn indicated enhanced electrochemical reaction, was the major contributor of improved  $\text{NH}_3$  production in the presence of nanoparticles. Unfortunately, however, the corresponding current efficiencies were rather poor: 0.18%, 0.14%, and 0.17% for control,  $\text{CoFe}_2\text{O}_4$ , and  $\text{Fe}_2\text{O}_3$ , respectively, mainly owing to  $\text{H}_2$  evolution from water electro-reduction. Slightly lower current efficiencies in the presence of nanocatalyst suspensions were observed, presumably because some of electrons were diverted to dendritic Fe or Co deposition on the working electrode [21-23].

Fig. 4 illustrates the schematic cross-sections of the reaction sites on the working electrode. In the absence of nanocatalysts, the surface of Ni working electrode (a) is the only available site where any reaction occurs. In the presence of nanoparticles suspended in molten chloride, two more sites become available to account for the catalytic role of nanocatalysts: a junction between the electrode and nanoparticles (b) and the surface of nanoparticles (c).

The junction between the electrode and nanocatalysts (b) is thought to provide excellent reaction sites where electrical conductivity and catalytic activity are both ensured [24]. In our experiment,

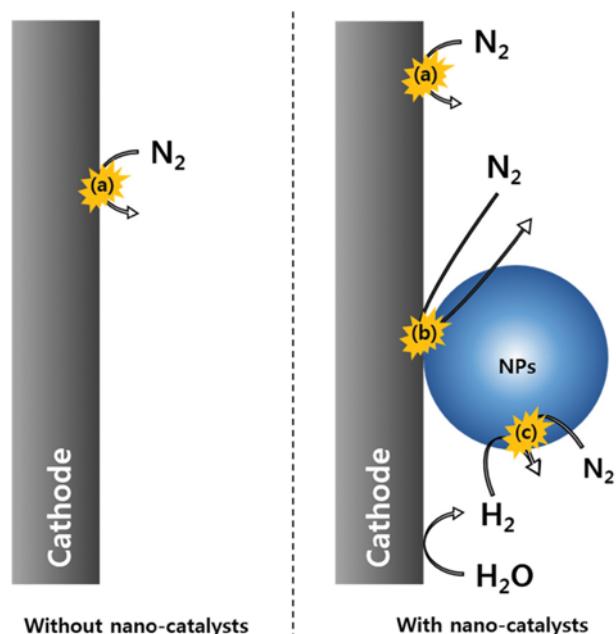


Fig. 4. Schematic cross-sections of the reaction sites on the working electrode with and without nano-catalysts.

$\text{N}_2$  might undergo enhanced electronation processes with the aid of nanocatalyst at this site (b), as can be inferred from the increased magnitude of current densities in the presence of nanoparticles. Recent similar studies, in fact, demonstrated the electro-catalytic activity of metal oxide suspension (especially  $\text{Fe}_2\text{O}_3$ ) on the electrochemical  $\text{N}_2$  reduction in molten hydroxide [2,16].

Another feasible mechanism is  $\text{NH}_3$  synthesis via a chemical reaction between  $\text{N}_2$  and  $\text{H}_2$ , which originated from the electro-reduction of water, namely  $\text{H}_2$  evolution [2]. This route is indeed plausible in that  $\text{Fe}_2\text{O}_3$  is a commonly used catalyst in the traditional H.B. process and its composites amended with Co have also been attempted for the improvement of catalytic activity and/or stability [25-27].

The catalytic activity of  $\text{Fe}_2\text{O}_3$  was found to be higher than  $\text{CoFe}_2\text{O}_4$  in terms of both current density and  $\text{NH}_3$  yield. Their activities could also be translated into the nanoparticle-induced increment in  $\text{NH}_3$  yield, that is, the difference in  $\text{NH}_3$  yield with and without nanocatalysts, normalized with mass of catalyst used:  $1.98 \times 10^{-6}$  mol  $\text{g}^{-1}$  and  $2.89 \times 10^{-6}$  mol  $\text{g}^{-1}$  for  $\text{CoFe}_2\text{O}_4$  and  $\text{Fe}_2\text{O}_3$ , respectively. Among a great many factors affecting catalytic performance, the Fe-Co alloy seemed to be critically dependent upon the ratio of Co to Fe for its  $\text{NH}_3$  synthesis activity [25-27]. The incorporation of an appropriate amount of Co, e.g., a molar ratio of Co : Fe = 5 : 95 according to Ref. [26], led to enhanced performance [26,27], and therefore the poorer performance of  $\text{CoFe}_2\text{O}_4$  arose from the use of a suboptimal content of basically inactive component Co, as reported in previous studies [26,27].

This study, though without rigorous optimization for reactor configuration and catalyst preparation, revealed that metal oxide nanoparticles, as either primary cocatalysts or mere catalysis enhancers, can be included to increase yield and speed of electrochemical synthesis of  $\text{NH}_3$  in molten chloride. The maximum  $\text{NH}_3$  syn-

thesis rate in this study ( $3.00 \times 10^{-10}$  mol s<sup>-1</sup> cm<sup>-2</sup>) using Fe<sub>2</sub>O<sub>3</sub> is lower than previously reported data obtained on the basis of molten salt, LiCl-KCl-CsCl ( $2.00 \times 10^{-8}$  mol s<sup>-1</sup> cm<sup>-2</sup> at 573 K) and NaOH-KOH ( $1.00 \times 10^{-8}$  mol s<sup>-1</sup> cm<sup>-2</sup> at 473 K) [2,10]; and of solid electrolyte, namely, Nafion ( $1.13 \times 10^{-8}$  mol s<sup>-1</sup> cm<sup>-2</sup> at 353 K) [1]. The issue of low performance of this molten-typed system is expected to further be resolved by way of not only the addition of more appropriate additives but also the continuous optimization of reactor configuration, enabling to avoid H<sub>2</sub> evolution and NH<sub>3</sub> back-oxidation on the anode. Over time, some of nanoparticles might coagulate or decompose in the form of ion, leading to dendritic deposition on the cathode [21-23], and these are related to the catalyst stability and thus must be investigated in the future.

## CONCLUSIONS

Nano-Fe<sub>2</sub>O<sub>3</sub> and CoFe<sub>2</sub>O<sub>4</sub> were suspended in molten salt of LiCl-KCl-CsCl and their potential applicability as nanocatalysts in this molten chloride-based NH<sub>3</sub> electro-synthesis was investigated. Overall performance, evaluated in terms of current density and NH<sub>3</sub> yield during potentiostatic electrolysis, was improved in the presence of nanocatalysts, with better performance observed using Fe<sub>2</sub>O<sub>3</sub> than CoFe<sub>2</sub>O<sub>4</sub>. The nanocatalysts were speculated to catalyze both the electrochemical N<sub>2</sub> reduction and chemical reaction between N<sub>2</sub> and water-derived H<sub>2</sub>, thereby resulting in enhanced NH<sub>3</sub> synthesis.

## ACKNOWLEDGEMENTS

This work was conducted under the framework of Research and Development Program of the Korea Institute of Energy Research (KIER) (B6-2442).

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