

## Potential organic magnetic nanoparticles from peel extract of *Archidendron pauciflorum* for the effective removal of cationic and anionic dyes

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**Abstract**—The adsorption of cationic (methylene blue, MB) and anionic (Congo red, CR) dyes using magnetic from *Archidendron pauciflorum* peel extract obtained via sonochemical synthesis ( $\text{Fe}_3\text{O}_4$ -AP) has been carried out. This study also compared the ability of  $\text{Fe}_3\text{O}_4$ -AP as an adsorbent for MB and CR through isotherm and kinetics studies.  $\text{Fe}_3\text{O}_4$ -AP was synthesized by the sonochemical method at a frequency of 800 kHz and characterized using FTIR, XRD, PSA, VSM and SEM-EDX. The XRD diffractogram showed  $\text{Fe}_3\text{O}_4$ -AP with high crystallinity with a crystal size of 17.05 nm, and the particle size distributed in three groups, 2.56, 862.23, and 4855.78 nm, respectively. Meanwhile, the Ms of  $\text{Fe}_3\text{O}_4$ -AP was 27.71 emu/g. The SEM-EDX showed disordered morphology with Fe, O and C elemental composition. The kinetics and isotherm of MB and CR dye adsorption on  $\text{Fe}_3\text{O}_4$ -AP followed Ho's kinetics model and Freundlich isotherm. The Freundlich isotherm model with adsorption capacities MB and CR on  $\text{Fe}_3\text{O}_4$ -AP was 16.02 and 10.24 mg/g, respectively.

Keywords: Magnetic Nanoparticles, *Archidendron pauciflorum* Peel Extract, Sonochemistry, Methylene Blue, Congo Red

### INTRODUCTION

Synthetic dyes such as methylene blue and Congo red are the most widely used dyes in the textile industry [1,2]. Mostly, in the coloring process of the textile industry, it is only 45% of the dye that is attached to the cloth, while the rest is wasted in the washing process. Synthetic dyes in wastewater are unnaturally degraded and even have toxic properties; as a consequence, they must be processed before being discharged into the environment [1,3,4].

Many materials have been developed to treat dyes in wastewater. However, in recent years, materials with magnetic properties have received more attention in environmental remediation for being easier to regenerate and separate using an external magnetic field. Of the magnetic materials being developed, the magnetite compound ( $\text{Fe}_3\text{O}_4$ ) is the most popular as it has a number of strong and more stable magnetic properties [5-11].

Plant extracts are some of the innovations of environmentally friendly magnetite synthesis. The specific content of organic compounds in plant extracts can act as the reducing agents and capping agents that control the growth process of material particles [12-14]. In addition, organic compounds can coat the magnetite materials' surface to prevent agglomeration [5,15,16]. The synthesis of magnetite nanomaterial using plant extracts has been widely developed using co-precipitation [17,18] and reverse co-precipitation [14,19]; however, the use of edible plant extracts will undermine food security.

*Archidendron pauciflorum* (Djengkol) plants are widely cultivated

in tropical areas, especially in Southeast Asia [20]. The fruit's flesh is used as a food product in great demand. Along with the great market demand, the amount of peel waste also increases. Thus, the waste used as an added-value product becomes interesting to develop because it contributes to the environmental impact less and does not interfere with food security. The peel contains many compounds of tannins, saponins, alkaloids, glycosides, flavonoids, and steroids/triterpenoids [19] that can act as the reducing agents and capping agents in magnetite synthesis.

In this study, the developed magnetite using the peel of *Archidendron pauciflorum* was applied as an adsorbent for methylene blue and Congo red dyes. The sonochemical method was used in the synthesis process to obtain a smaller particle size. This method facilitates microscopic particle growth because the flow of ultrasonic waves can cause acoustic cavitation, which is the formation, growth, and bursting of liquid bubbles at very high temperatures and pressures (5,000 K, 20 MPa), followed by very high cooling rates (1010 K/S), resulting in extreme conditions. This extreme condition then leads to microscopic particle growth [21]. Magnetite synthesis using sonochemical method has been widely developed, but the synthesis of magnetite based on plant extracts using sonochemical methods has not been widely reported. In this research, the effectiveness of the developed magnetite using the peel of *Archidendron pauciflorum* obtained via sonochemical method for methylene blue and Congo red dyes adsorbent was studied through kinetics and adsorption isotherms.

### EXPERIMENTAL

#### 1. Materials

The plant waste used was *Archidendron pauciflorum* (locally called

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as djengkol) peel and the peel was further called as AP peel. The chemicals purchased from Merck Co were iron(III)chloride hexahydrate ( $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ ), iron(II)sulfate heptahydrate ( $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ ), sodium hydroxide ( $\text{NaOH}$ ), hydrochloric acid ( $\text{HCl}$ ), methylene blue and Congo red. The solvent used was water with twice distillation (aquabidest) from PT. Ikapharmindo.

## 2. Preparation of *Archidendron Pauciflorum* Peel Extract

The peel was dried in an oven at  $60^\circ\text{C}$  for 2 hours, then cut into small pieces and mashed into powder. The organic compounds from peel powder were extracted using water as a solvent for 20 minutes at a temperature of  $60^\circ\text{C}$ . The peel extract was then separated from the residue, and stored in the refrigerator. Before being used for synthesis, the extract must be left at a room temperature.

## 3. Sonochemical Synthesis of $\text{Fe}_3\text{O}_4$ -AP

The magnetite produced from the peel of *Archidendron pauciflorum* using the sonochemical method was further named  $\text{Fe}_3\text{O}_4$ -AP. The sonicator used was the Leistungsfreq (generator type with a primary voltage of 230 V 50/60 Hz). A mixture of  $\text{Fe}^{3+}$  and  $\text{Fe}^{2+}$  precursors in a ratio of 2:1 was prepared by dissolving 2.164 g  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  and 1.112 g  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  with 100 mL aquabidest and then added to the  $\text{NaOH}$  1 M solutions (1.6 g, 40 mL) by dropping them slowly. After the mixture of  $\text{Fe}^{3+}$  and  $\text{Fe}^{2+}$  precursors was dripped, the peel extract was poured. Stirring was continued for 60 minutes at a room temperature with an ultrasonic wave stream of 800 kHz. The precipitate and filtrate were separated by centrifugation using an external magnetic field.

## 4. Characterization of $\text{Fe}_3\text{O}_4$ -AP

The  $\text{Fe}_3\text{O}_4$ -AP was characterized using FTIR, XRD, PSA, VSM and SEM-EDX. Functional group analysis used FTIR spectrophotometer (Shimadzu Prestige 21) in the transmission mode as the KBr method was used for all the powders. Crystallinity and crystal size of  $\text{Fe}_3\text{O}_4$ -AP, meanwhile, were determined using X-Ray diffraction (XRD-6000 Shimadzu) patterns recorded using a Bruker D2 phase diffractometer with  $\text{Cu K}\alpha$  ( $\lambda=0.1546$  nm) radiation. Further, the particle size was determined by particle size analyzer (PSA) (Horiba SZ-100). The magnetization saturation of  $\text{Fe}_3\text{O}_4$ -AP was conducted using a vibrating sample magnetometer (VSM) and the analysis of morphology or surface structure and elemental content of  $\text{Fe}_3\text{O}_4$ -AP used scanning electron microscope-energy dispersive X-ray (SEM-EDX).

### 4-1. Determination of the Maximum Wavelength of MB and CR Dye Solutions

The MB and CR wavelengths were measured in the 400-700 nm wavelength range. Maximum wavelength information was used to construct the standard curves of MB and CR solutions. From the linear equations of the MB and CR standard curves, the concentrations of residual as well as the adsorbed MB and CR dyes could be then calculated.

## 5. Dye Adsorption Studies

MB and CR adsorption studies on  $\text{Fe}_3\text{O}_4$ -AP were performed by interacting MB and CR with  $\text{Fe}_3\text{O}_4$ -AP at various pH, adsorption time, and initial concentration of MB and CR.

### 5-1. pH Effect

A total of 25 mL of MB and CR dye solutions with a concentration of 15 ppm with a solution pH of 2, 4, 6, 8 and 10 interacted with 10 mg of  $\text{Fe}_3\text{O}_4$ -AP adsorbent for 60 minutes at room tempera-

ture. The adsorbent and filtrate of the mixture were separated by centrifugation using an external magnetic field. The amount of residual dye contained in the filtrate was analyzed using a UV-Vis spectrophotometer. The dye removal efficiency percentage (R%) was obtained from Eq. (1).

$$R(\%) = \left( \frac{C_0 - C_e}{C_0} \right) \times 100\% \quad (1)$$

## 6. Contact Time Effect and Kinetics Study

In the kinetic studies, the dye adsorption rate on the adsorbent surface and the mechanism between the dye and the adsorbent were evaluated. The adsorption kinetics of MB and CR on  $\text{Fe}_3\text{O}_4$ -AP was studied by interacting 10 mg of adsorbent  $\text{Fe}_3\text{O}_4$ -AP with 25 mL of MB dye and 15 ppm CR for 5-90 minutes. The interaction was carried out using the optimum dye pH and at room temperature. In this study, the three kinetic models used included Lagergren's pseudo-first-order, Ho's pseudo-second order, and Elovich's kinetic models.

## 7. Initial Dye Concentration Effect and Adsorption Isotherms Models

MB and CR adsorption isotherms on  $\text{Fe}_3\text{O}_4$ -AP were studied by interacting 10 mg of  $\text{Fe}_3\text{O}_4$ -AP adsorbent with MB and CR dyes of 5, 10, 15, 25 and 50 ppm, respectively, at room temperature with optimum dye pH and optimum reaction time. The adsorption capacity increased nonlinearly with increasing initial concentration [22].

## RESULTS AND DISCUSSION

### 1. Characterization of $\text{Fe}_3\text{O}_4$ -AP

The presence of functional groups in  $\text{Fe}_3\text{O}_4$ -AP can affect the adsorption ability of dyes [23]. The result of FTIR spectrophotometry was used to determine the type of functional group possessed by  $\text{Fe}_3\text{O}_4$ -AP. Based on the FTIR spectra as shown in Fig. 1, the functional groups of  $\text{Fe}_3\text{O}_4$ -AP could be derived from the func-

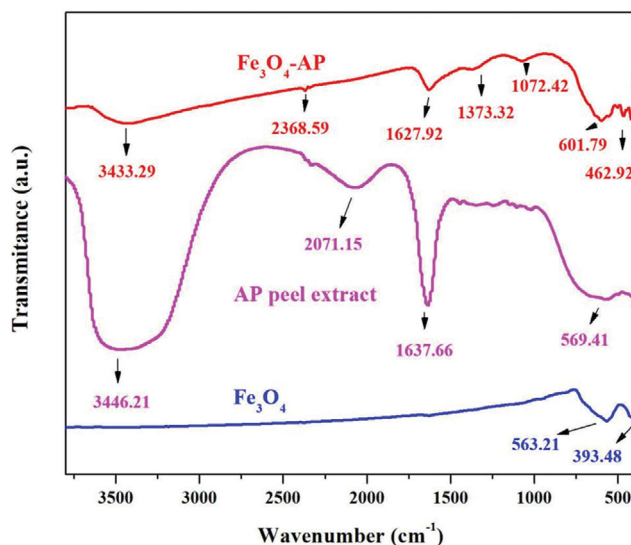


Fig. 1. FTIR spectra of pure  $\text{Fe}_3\text{O}_4$ , *Archidendron pauciflorum* peel extract and  $\text{Fe}_3\text{O}_4$ -AP.

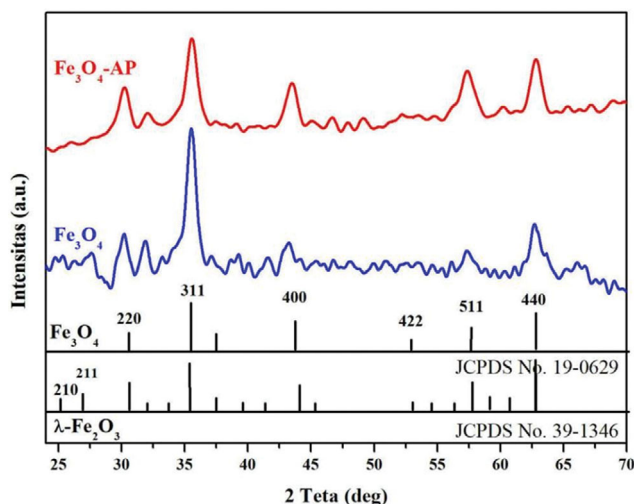


Fig. 2. XRD pattern of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4\text{-AP}$ .

tional groups of pure  $\text{Fe}_3\text{O}_4$  and AP peel extract. Absorption at wave numbers of 462.92 and 601.79  $\text{cm}^{-1}$  in  $\text{Fe}_3\text{O}_4\text{-AP}$  indicated the presence of  $\text{Fe}_3\text{O}_4$  in the form of Fe-O bonds. Compared to pure  $\text{Fe}_3\text{O}_4$  spectra, an absorption shift was observed due to the interaction between the pure  $\text{Fe}_3\text{O}_4$  surface and organic compounds in the AP peel extract. On the other hand, the absorption at the wave number of 462.92  $\text{cm}^{-1}$  showed Fe-O bonds in octahedral units, while the absorption at 601.79  $\text{cm}^{-1}$  showed Fe-O bonds in tetrahedral units [16,19,24,25].

The presence of functional groups of organic compounds derived from AP peel extract was indicated by the appearance of absorption at wave numbers 1,072.42, 1,373.32, 1,627.92, 2,368.59 and 3,433.29  $\text{cm}^{-1}$ . These absorptions indicated the presence of C-O stretching vibrations, C=C aromatic compounds,  $-\text{CH}_2$  stretching, and -OH group vibrations of carboxylic acids, alcohols, and phenols [26-28]. Though again there were absorption shifts due to new interactions compared to the AP peel extract, those indicated that  $\text{Fe}_3\text{O}_4\text{-AP}$  magnetic particles had been successfully synthesized

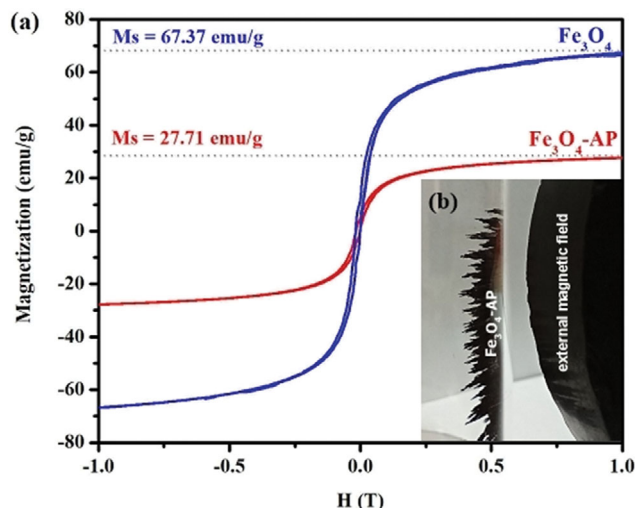


Fig. 3. (a) Magnetic properties of  $\text{Fe}_3\text{O}_4\text{-AP}$  (b) Magnetization curve at room temperature for  $\text{Fe}_3\text{O}_4\text{-AP}$ .

from AP peel extract.

XRD characterization was carried out to determine the crystal structure of  $\text{Fe}_3\text{O}_4\text{-AP}$  as presented in Fig. 2. The  $\text{Fe}_3\text{O}_4\text{-AP}$  diffractogram showed the presence of intense peaks at the values of  $2\theta$  (Miller index) 30° (220), 35° (311), 43° (400), 53° (422), 57° (511), and 62° (440). These characteristic peaks belonged to  $\text{Fe}_3\text{O}_4$  (JCPDS No. 19-0629). This confirmed that the magnetite ( $\text{Fe}_3\text{O}_4$ ) formed did not mix with other iron oxides such as  $\text{Fe}_2\text{O}_3$  (JCPDS No. 39-1346). This type of iron oxide led to stronger magnetic properties; it is thus more desirable as an adsorbent.

Fig. 3(a) shows the saturation magnetization (Ms) value of  $\text{Fe}_3\text{O}_4\text{-AP}$ . The presence of  $\text{Fe}_3\text{O}_4$  in the AP peel extract contributed to a phenomenon of magnetization. The lower saturation magnetization observed for the AP peel extract during magnetite synthesis compared to the  $\text{Fe}_3\text{O}_4$  was reasonable since the magnetization vectors for all domains in extensive materials such as AP peel extract containing various phenolic compounds could not be completely

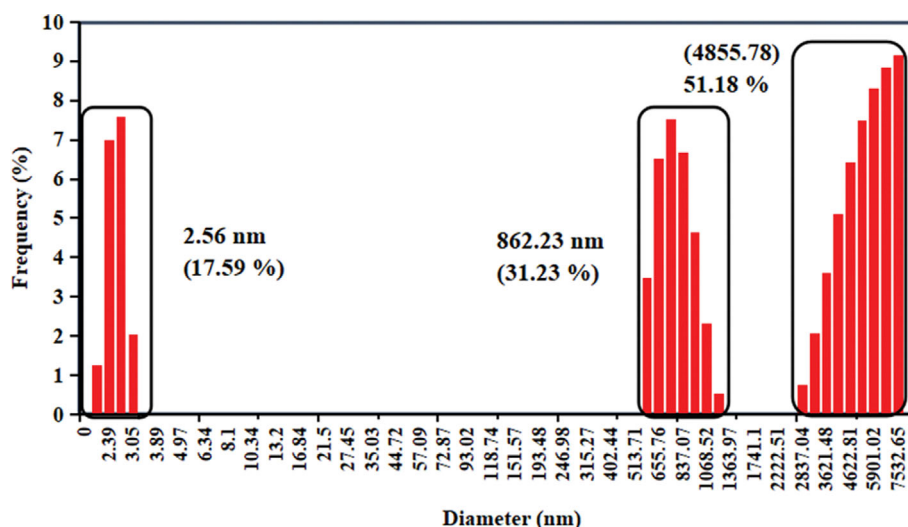
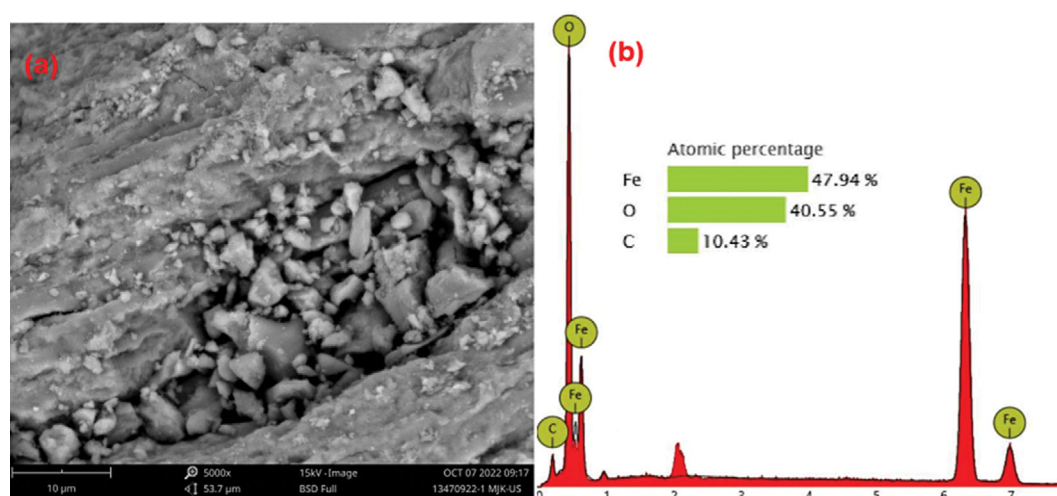


Fig. 4. Particle size distribution of  $\text{Fe}_3\text{O}_4\text{-AP}$ .

**Table 1. Data of some plant-based magnetite particles**

Extract source	Synthesis condition	Particle size (nm)	Morphology	Reference
<i>Hevea brasiliensis</i> Muell. Arg. peel	Conventional method Room temperature (27 °C), 1 h, FeCl <sub>3</sub> and FeCl <sub>2</sub>	200 nm	-	[25]
Tea dregs	Conventional method pH 11, 60 min, 60 °C	2,670.37 nm	-	[29]
<i>Archidendron</i> <i>pauciflorum</i>	Conventional method, 60 min, 60 °C, FeSO <sub>4</sub> ·7H <sub>2</sub> O, FeCl <sub>3</sub> ·6H <sub>2</sub> O	318 and 294 nm	-	[19]
<i>Archidendron</i> <i>pauciflorum</i>	Sonochemical method, 60 min, 60 °C, FeSO <sub>4</sub> ·7H <sub>2</sub> O, FeCl <sub>3</sub> ·6H <sub>2</sub> O	2.56 nm, 862.23 nm, and 4,855.78 nm	Rough surface	This research

**Fig. 5. (a) SEM images of Fe<sub>3</sub>O<sub>4</sub>-AP and (b) energy-dispersive X-ray fluorescence spectrometry spectra of Fe<sub>3</sub>O<sub>4</sub>-AP.**

harmonized. Fig. 3(b) illustrates an image of Fe<sub>3</sub>O<sub>4</sub>-AP attracted to a magnetic field. The goal is to facilitate the separation process between the adsorbent and filtrate using an external magnetic field. The crystal size of Fe<sub>3</sub>O<sub>4</sub>-AP was determined using Debye-Scherrer's equation with full width at half maximum (FWHM=0.461) of the (311) reflection. The crystal size of Fe<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>O<sub>4</sub>-AP obtained in this study was 15.00 nm and 17.05 nm, respectively.

Fig. 4 presents the particle size distribution of Fe<sub>3</sub>O<sub>4</sub>-AP that was not uniform. There were three size groups with an average size of 2.56 nm, 862.23 nm, and 4,855.78 nm. Table 1 presents the comparison of particle size of the Fe<sub>3</sub>O<sub>4</sub>-AP with other magnetite particles. Compared to the previous studies, the sonochemical method succeeded in synthesizing Fe<sub>3</sub>O<sub>4</sub>-AP nanoparticles with smaller size, i.e., 2.56 nm.

Fig. 5(a) shows characterization results using SEM-EDX, and the image confirms the previous finding of using particle size analysis (PSA), as the magnetite particle size was here observed in the range of 1-5 μm. Fig. 5(b) shows the elemental content of Fe<sub>3</sub>O<sub>4</sub>-AP. The most significant percentage of elements was Fe, followed by O and C. This also reveals the role of Fe<sub>3</sub>O<sub>4</sub> presence in the synthesis.

## 2. Synthesis Mechanism of Fe<sub>3</sub>O<sub>4</sub>-AP

Fe<sub>3</sub>O<sub>4</sub>-AP was synthesized using the reverse co-precipitation method at pH 12. The pH conditions of the synthesis greatly affected

the purity of the Fe<sub>3</sub>O<sub>4</sub>-AP obtained. If the synthesis was conducted above pH 12, the iron oxide formed was magnetite (Fe<sub>3</sub>O<sub>4</sub>). Furthermore, if the synthesis was carried out below pH 8, other iron oxides such as hematite (Fe<sub>2</sub>O<sub>3</sub>) would be formed. According to the Pourbaix diagram of iron oxide, Fe<sub>3</sub>O<sub>4</sub> is stable at pH 8 and Fe<sub>2</sub>O<sub>3</sub> at pH 3 [19].

The original magnetite compounds had a pH<sub>PZC</sub>=6-6.8 and the synthesis or modification method using organic compounds caused the pH<sub>PZC</sub> magnetite to decrease into pH 3-4. The decrease in the pH<sub>PZC</sub> value was caused by the protonation and deprotonation mechanism of the carboxylic acid group and the phenol hydroxy group with metal oxide nanoparticles [30-33].

In this study, Fe<sub>3</sub>O<sub>4</sub>-AP was synthesized at pH>pH<sub>PZC</sub> Fe<sub>3</sub>O<sub>4</sub>. Under this condition, the surface of the magnetite was negatively charged. High solution pH (basic conditions) caused hydroxy ions (OH<sup>-</sup>) to dominate in solution and then was able to extract H<sup>+</sup> from Fe-OH to produce negatively charged iron oxide species (Fe-O<sup>-</sup>), as shown in Eq. (2) [34].

The negative surface of magnetite (Fe-O<sup>-</sup>) will be able to interact with organic compounds such as tannins, flavonoids, and saponins through hydrogen bonds. Electrostatic interactions are difficult in this condition because these organic compounds' carboxylate and hydroxy groups have been protonated to -COO<sup>-</sup> and -O<sup>-</sup>



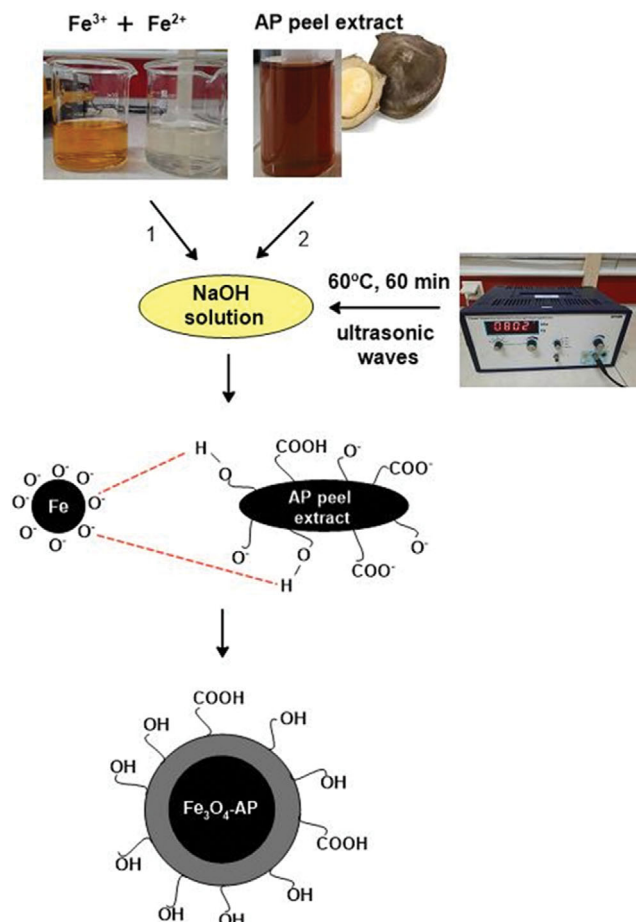


Fig. 6. Illustration of  $\text{Fe}_3\text{O}_4\text{-AP}$  synthesis.

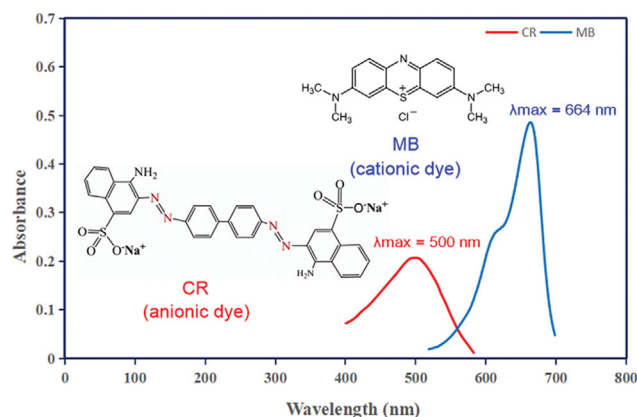


Fig. 7. Absorbance data of CR and MB dyes at various wavelengths.

[19]. Fig. 6 illustrates the synthesis mechanism of  $\text{Fe}_3\text{O}_4\text{-AP}$  as previously described.

### 3. Structure and Maximum Wavelength of the Dye

Fig. 7 presents the graphs of the wavelengths of CR and MB dyes. The determination of the peak wavelength of dye was required to evaluate the concentration of dye adsorbed on  $\text{Fe}_3\text{O}_4\text{-AP}$ . The peak wavelength of CR dyes was 500 nm, while the maximum wavelength of MB was 664 nm.

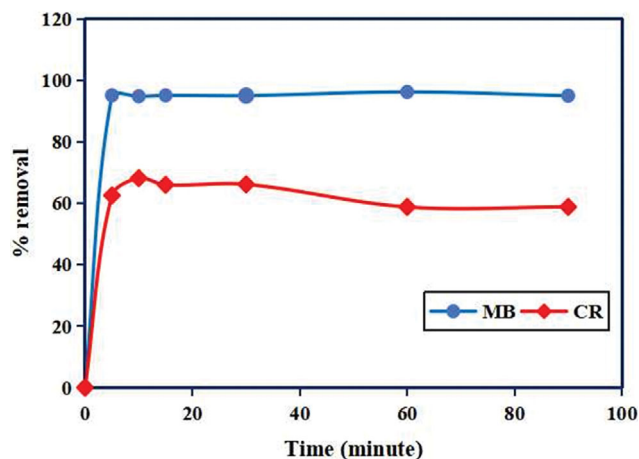


Fig. 8. Kinetic profile of adsorption of MB and CR (pH 4, [MB or CR]=15 ppm and room temperature) using  $\text{Fe}_3\text{O}_4\text{-AP}$ .

### 4. Adsorption Study of Cationic and Anionic Dyes on $\text{Fe}_3\text{O}_4\text{-AP}$

#### 4-1. Kinetic Profile of the MB and CR Adsorption on $\text{Fe}_3\text{O}_4\text{-AP}$

The kinetic profile of MB and CR adsorption using  $\text{Fe}_3\text{O}_4\text{-AP}$  had a similar pattern as shown in Fig. 8. Adsorption occurred rapidly in the early minutes until the fifth minute equilibrium was reached. After reaching equilibrium, there was no significant increase or decrease in MB or CR removal. The surface condition of  $\text{Fe}_3\text{O}_4\text{-AP}$  at the beginning of the interaction was still unsaturated, thus allowing the abundant active groups in  $\text{Fe}_3\text{O}_4\text{-AP}$  to interact very quickly with MB and CR. After reaching equilibrium, the surface of  $\text{Fe}_3\text{O}_4\text{-AP}$  became saturated; hence, the adsorption of MB and CR no longer increased. It was also observed that the ability of  $\text{Fe}_3\text{O}_4\text{-AP}$  to adsorb MB was better than CR due to differences in the chemical structure of MB and CR related to the previous pH discussion. Further explanation regarding these findings would be further confirmed through studies of kinetics and isotherms adsorption.

#### 4-2. Effect of Dye Initial Concentration on the Adsorption Ability of $\text{Fe}_3\text{O}_4\text{-AP}$

Fig. 9 presents the relationship between the initial concentrations of MB and CR and the adsorption ability of  $\text{Fe}_3\text{O}_4\text{-AP}$ . The adsorption of MB and CR on  $\text{Fe}_3\text{O}_4\text{-AP}$  increased until the initial concentration of MB and CR reached 15 ppm. However, the adsorption ability of  $\text{Fe}_3\text{O}_4\text{-AP}$  decreased, at which the initial dye concentration was higher than 15 ppm. The decrease in % removal at the initial dye concentration  $\geq 15$  ppm was because, at high concentrations, the dyes would compete with each other to interact with the  $\text{Fe}_3\text{O}_4\text{-AP}$  adsorbent. The optimum % removal of MB and CR was 97 and 91%, respectively.

#### 4-3. Effect of Dye pH on $\text{Fe}_3\text{O}_4\text{-AP}$ Adsorption Ability

Fig. 10 presents the results of the pH optimization for dye removal by  $\text{Fe}_3\text{O}_4\text{-AP}$ . The  $\text{Fe}_3\text{O}_4\text{-AP}$  adsorbent had a  $\text{pH}_{\text{PZC}}=3$ . The surface conditions of  $\text{Fe}_3\text{O}_4\text{-AP}$  at pH above and below  $\text{pH}_{\text{PZC}}$  were different. Various previous studies have reported that a solution's initial pH conditions greatly affected a magnetic particle's adsorption ability [35-37]. It is reported for pH above  $\text{pH}_{\text{PZC}}$ , the surface of  $\text{Fe}_3\text{O}_4\text{-AP}$  was negatively charged due to the deprotonation of

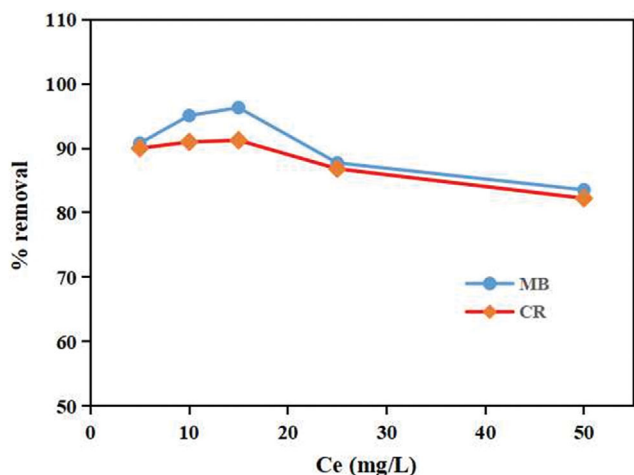


Fig. 9. Adsorption of MB and CR at various dye initial concentrations (pH 4,  $t=30$  min, room temperature).

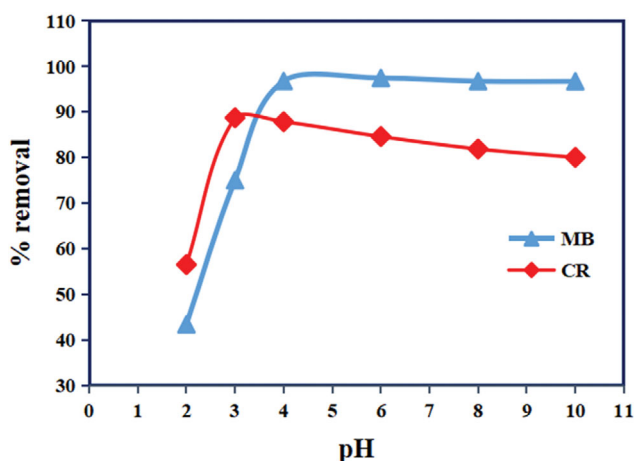


Fig. 10. pH optimization for dye removal by  $\text{Fe}_3\text{O}_4\text{-AP}$ .

-OH and -COOH groups into  $-\text{O}^-$  and  $-\text{COO}^-$  groups. For pH under  $\text{pH}_{\text{PZC}}$  the surface of  $\text{Fe}_3\text{O}_4\text{-AP}$  was positively charged due to the protonation of the -OH and -COOH groups into  $-\text{OH}_2^+$  and  $-\text{COOH}_2^+$  groups [18,19]. Thus, the difference in the surface charge of the adsorbent affected the ability of  $\text{Fe}_3\text{O}_4\text{-AP}$  to adsorb dyes as here caused by pH. As observed in Fig. 8, MB dye adsorption using  $\text{Fe}_3\text{O}_4\text{-AP}$  led to a great performance of % removal at  $\text{pH}>3$ , and the ability of adsorption decreased at  $\text{pH}<3$ . It was plausible because MB is a cationic dye with  $\text{S}^+$  or  $\text{N}^+$  groups, thus easily interacting through electrostatic connections with  $-\text{O}^-$  and  $-\text{COO}^-$  groups on the surface of  $\text{Fe}_3\text{O}_4\text{-AP}$  which were negatively charged at  $\text{pH}>3$ ; hence, MB adsorption on  $\text{Fe}_3\text{O}_4\text{-AP}$  could reach 96-97%. Meanwhile, at  $\text{pH}\leq 3$ , % MB removal was only around 43-75%. At this pH condition, the surface of  $\text{Fe}_3\text{O}_4\text{-AP}$  was positively charged; thus, electrostatic interactions between  $\text{S}^+$  or  $\text{N}^+$  of MB with  $-\text{OH}_2^+$  and  $-\text{COOH}_2^+$   $\text{Fe}_3\text{O}_4\text{-AP}$  groups were increasingly difficult to occur.

The adsorption of CR on  $\text{Fe}_3\text{O}_4\text{-AP}$  was found better than the adsorption of MB on  $\text{Fe}_3\text{O}_4\text{-AP}$  at a pH below  $\text{pH}_{\text{PZC}}$   $\text{Fe}_3\text{O}_4\text{-AP}$ . CR is an anionic dye with  $\text{SO}_3^-$  groups, thus making it easier to interact with the positive  $\text{Fe}_3\text{O}_4\text{-AP}$  surface ( $\text{pH}<3$ ) through elec-

trostatic interactions between the  $\text{SO}_3^-$  groups of CR dyes with  $-\text{OH}_2^+$  and  $-\text{COOH}_2^+$  from the  $\text{Fe}_3\text{O}_4\text{-AP}$  adsorbent. Above pH 3, the ability of  $\text{Fe}_3\text{O}_4\text{-AP}$  to adsorb CR decreased because the -OH and -COOH groups of the  $\text{Fe}_3\text{O}_4\text{-AP}$  adsorbent had been deprotonated into  $-\text{O}^-$  and  $-\text{COO}^-$  groups; hence, electrostatic interactions were increasingly challenging to occur. However, the percentage of the removal was still above 80%. From this phenomenon, it was suspected that the electrostatic interaction mechanism was not the only mechanism between MB and CR with  $\text{Fe}_3\text{O}_4\text{-AP}$ .

Other possible interaction models were hydrogen bonding,  $\pi$ - $\pi$  interactions and hydrophobic interactions [38-40,50]. Hydrogen bonds occur between the hydrogen atoms of the  $-\text{OH}_2^+$  and  $-\text{COOH}_2^+$   $\text{Fe}_3\text{O}_4\text{-AP}$  groups with the nitrogen atoms of the  $-\text{N}(\text{CH}_3)_2$  group of MB or between the oxygen atoms of the  $-\text{O}^-$  and  $-\text{COO}^-$  groups and the hydrogen atoms of the  $-\text{CH}_2$  and  $-\text{NH}_2$  groups of CR. Meanwhile,  $\pi$ - $\pi$  interactions occur between  $\pi$  bonds in  $\text{Fe}_3\text{O}_4\text{-AP}$  due to the delocalization of the charge distribution of the conjugated aromatic ring with bonds in the aromatic ring of MB or CR dyes.

On the other hand, hydrophobic interaction is an interesting proposed mechanism because of the interaction between a hydrophobic molecule and dye molecules in an aqueous solution. When  $\text{Fe}_3\text{O}_4\text{-AP}$  (hydrophobic) meets aqueous solution molecules (MB and CR), hydrogen bonds will be broken between aqueous solution molecules to provide a space for  $\text{Fe}_3\text{O}_4\text{-AP}$ . However, aqueous solution molecules do not react with  $\text{Fe}_3\text{O}_4\text{-AP}$ . This process is considered as an endothermic reaction because heat will enter the system when a bond is broken. Furthermore, the aqueous solution molecules are distorted due to the presence of  $\text{Fe}_3\text{O}_4\text{-AP}$  molecules that form new hydrogen bonds between the aqueous solution molecules and further yield a clathrate cage around the  $\text{Fe}_3\text{O}_4\text{-AP}$  molecules. Fig. 11 illustrates the interaction mechanism between  $\text{Fe}_3\text{O}_4\text{-AP}$  with cationic and anionic dyes. The illustration is also strengthened by the post-adsorption  $\text{Fe}_3\text{O}_4\text{-AP}$  characterization results using an FTIR spectrophotometer as presented in Fig. 12. Since there was no new absorption peak in the post-adsorption of MB and CR on  $\text{Fe}_3\text{O}_4\text{-AP}$  spectra, the interaction between MB and CR with  $\text{Fe}_3\text{O}_4\text{-AP}$  occurred through physical interactions.

#### 4-4. Kinetics Studies

In this study, the three kinetic models used included Lagergren's pseudo-first-order, Ho's pseudo-second order, and Elovich's kinetic models. Lagergren's equation of pseudo-first order is presented in Eq. (3). The adsorption capacity of MB and CR dyes on  $\text{Fe}_3\text{O}_4\text{-AP}$  at time  $t$  (minutes) and equilibrium are expressed by  $q_t$  and  $q_e$  (mg/g), and the pseudo-first-order reaction rate constant is expressed by  $k_1$  ( $\text{min}^{-1}$ ). If a graph of  $\ln(q_e - q_t)$  versus  $t$  were made, it would produce a straight line with slope and intercept. The value of  $k_1$  was obtained from the slope, and the value of  $q_e$  was obtained from the intercept.

$$\ln(q_e - q_t) = \ln q_e - k_1 t \quad (3)$$

Ho's pseudo-second-order equation is expressed in Eq. (4). Like Lagergren's pseudo-first-order equation, the adsorption capacities of MB and CR dyes on  $\text{Fe}_3\text{O}_4\text{-AP}$  at time  $t$  (minutes) and equilibrium are expressed by  $q_t$  and  $q_e$  (mg/g), respectively. For Ho's pseudo-second-order, the constant is expressed by  $k_2$  (g/mg.min). The advantage of this model is that it could calculate the initial dye

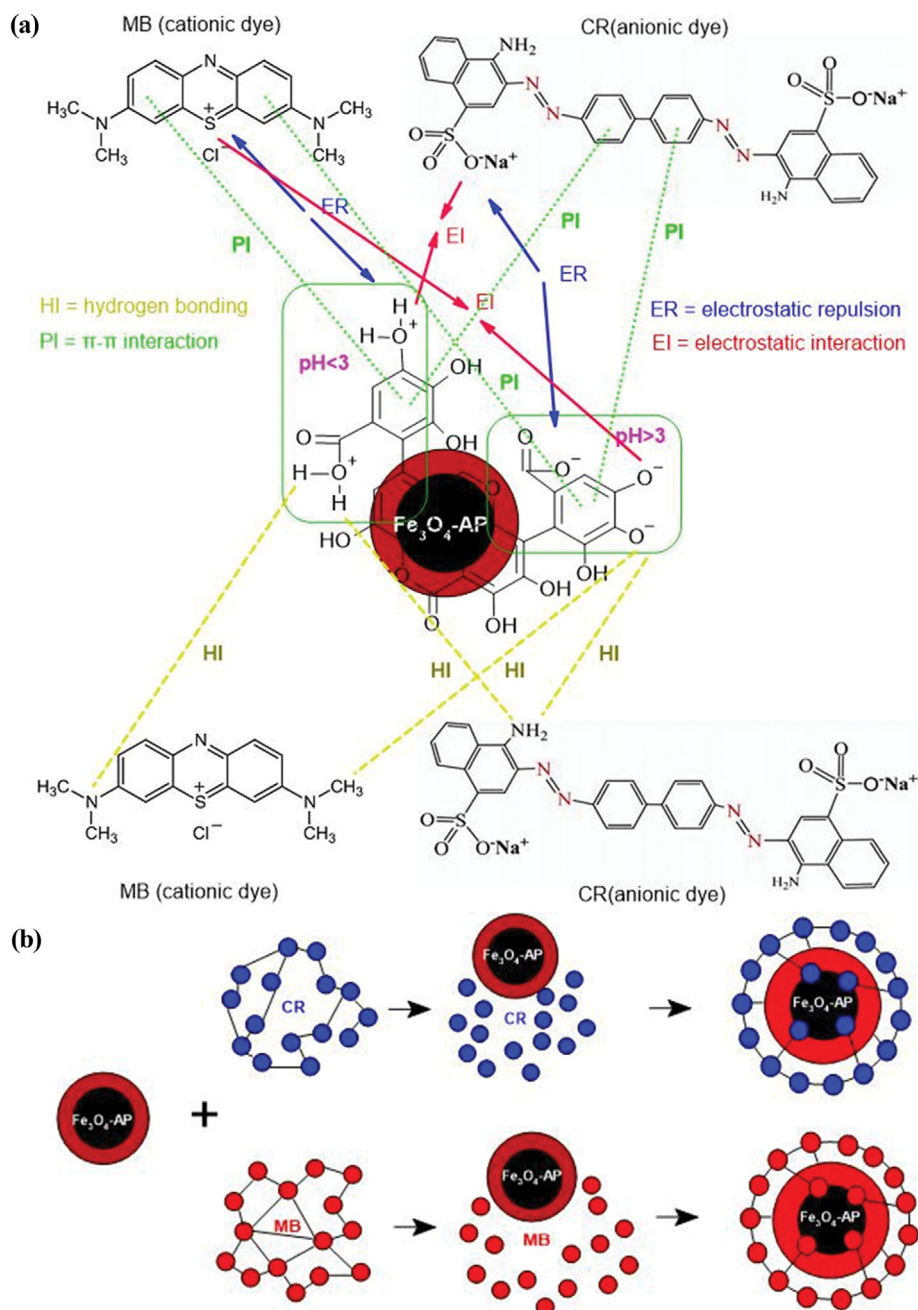


Fig. 11. Illustration of the interaction mechanism between Fe<sub>3</sub>O<sub>4</sub>-AP with cationic and anionic dyes.

adsorption rate on Fe<sub>3</sub>O<sub>4</sub>-AP (mg/g.min) with the formula presented in Eq. (5). The values of  $q_e$  and  $k_2$  were determined from the slope and intercept of the graph of  $t/q_t$  versus  $t$ .

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \quad (4)$$

$$h = k_2 q_e^2 \quad (5)$$

Elovich's kinetic model is expressed in Eq. (5). This kinetic model is suitable for the adsorption of gases and wastewater pollutants [41]. The desorption constant associated with the surface area and chemisorption activation energy is expressed by  $\beta$  (g/mg), and the

initial adsorption rate is expressed by  $\alpha$  (mg/g min). By making a graph of  $\ln t$  versus  $q_t$ , the  $\alpha$  and  $\beta$  values are determined from the slope and intercept.

$$q_t = \left( \frac{1}{\beta} \right) \ln(\alpha \beta) + \left( \frac{1}{\beta} \right) \ln(t) \quad (6)$$

Fig. 13 and Table 2 presents the graphs of the MB and CR adsorption kinetic models on Fe<sub>3</sub>O<sub>4</sub>-AP. Kinetic studies showed that the adsorption of MB and CR on Fe<sub>3</sub>O<sub>4</sub>-AP followed the pseudo-second-order Ho's kinetic model with  $R^2$  values of 1 and 0.9965, respectively, and did not match with the Lagergren pseudo-first-order kinetic model with  $R^2$  of 0.1959 and 0.098, respectively. These indi-

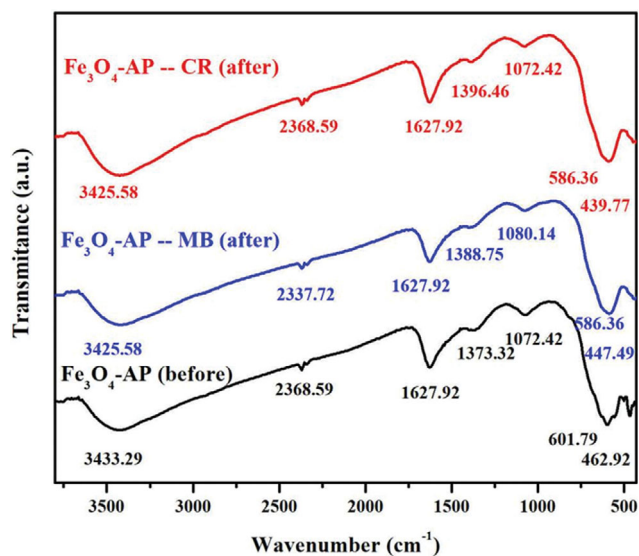


Fig. 12. FTIR spectra of  $\text{Fe}_3\text{O}_4\text{-AP}$  before and after adsorption.

cated that the adsorption of MB and CR involved more than two active sites belonging to the  $\text{Fe}_3\text{O}_4\text{-AP}$  surface [42]. In addition, the adsorption of MB and CR on  $\text{Fe}_3\text{O}_4\text{-AP}$  was determined by the adsorbent, adsorbate and water solvent used. The kinetics study of MB and CR adsorption on  $\text{Fe}_3\text{O}_4\text{-AP}$  using the Elovich model resulted in  $R^2$  values of 0.6504 and 0.5851, respectively, meaning that the adsorption of MB and CR on  $\text{Fe}_3\text{O}_4\text{-AP}$  also did not fol-

Table 2. Kinetic parameters of MB and CR dyes

Kinetic models	Parameters	Dyes	
		MB	CR
Lagergren's pseudo-first-order	$R^2$	<b>0.1959</b>	<b>0.098</b>
	$q_e$ (mg/g)	0.960	2.330
	$k$ ( $\text{min}^{-1}$ )	0.001	0.0166
Ho's pseudo-second-order	$R^2$	<b>1.0000</b>	<b>0.9965</b>
	$q_e$ (mg/g)	1,666.67	1,250.00
	$h$ (mg/g·min)	14,285.71	1,666.67
Elovich	$k$ (g/mg·min)	0.00514	0.00107
	$R^2$	<b>0.6504</b>	<b>0.5851</b>
	$\alpha$ (mg/g·min)	0.804	0.773
	$\beta$ (g/mg)	0.003	0.004

low this kinetic model. Elovich's kinetic model assumes that dye adsorption on  $\text{Fe}_3\text{O}_4\text{-AP}$  occurs at a local site, interactions between dye ions are possible, and dye concentration is considered to be constant [41]. The results of this kinetic study reinforced the presumption of the previously described interaction mechanism.

#### 4-5. Isotherm Studies

The adsorption isotherm was studied to determine the relationship between the initial concentrations of MB and CR dyes and the adsorption capacity of  $\text{Fe}_3\text{O}_4\text{-AP}$  when the dye was initially distributed in equilibrium between the solid and liquid phases. In this

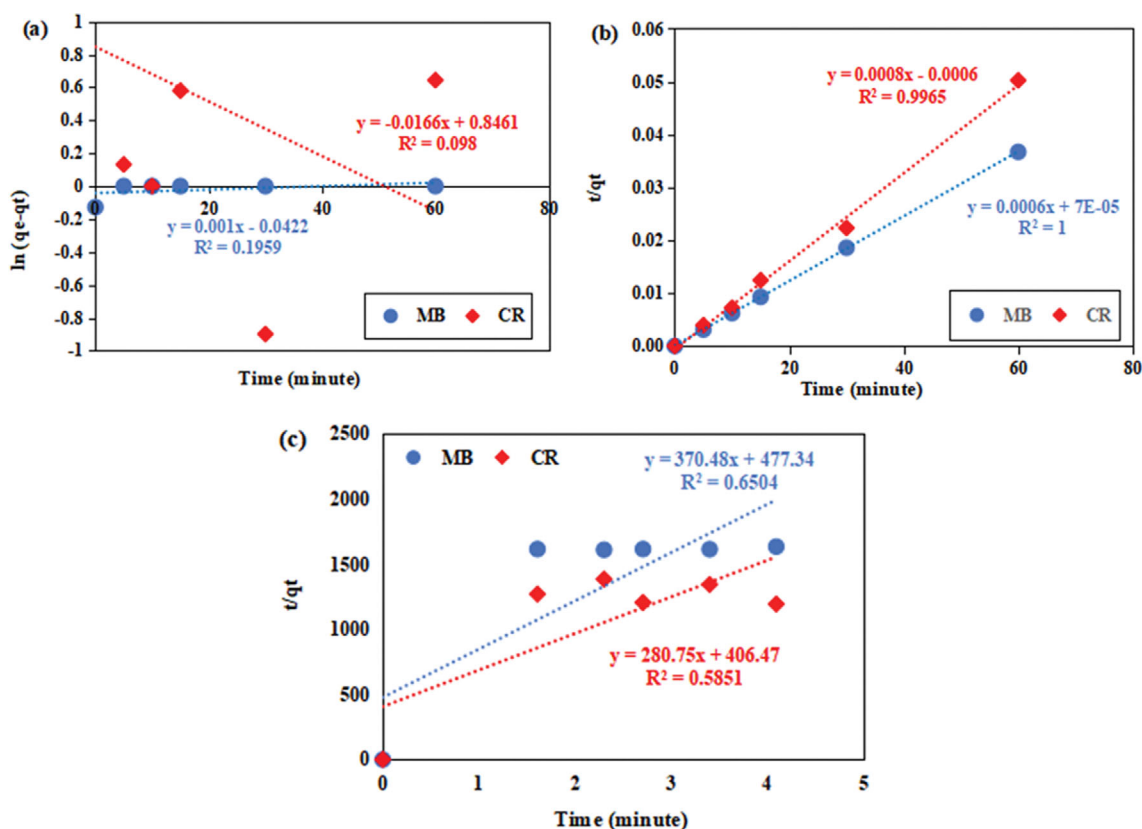


Fig. 13. (a). Lagergren's pseudo first-order (b) Ho's pseudo second (c) Elovich's kinetic models of MB and CR adsorption onto  $\text{Fe}_3\text{O}_4\text{-AP}$ .



study, three adsorption isotherm models were used: Langmuir, Freundlich and Temkin isotherm.

Langmuir isotherm model is expressed in Eq. (7) and the concentration of free dye ions in solution at equilibrium is expressed as  $C_e$  (mg/L). The amount of dye adsorbed at equilibrium and the maximum single-layer adsorption capacity is expressed by  $q_e$  and  $q_{max}$  (mg/g), respectively. Meanwhile,  $K_L$  is the Langmuir constant associated with the adsorption energy, describing the affinity of the dye for  $Fe_3O_4$ -AP (L/mg). By plotting  $C_e/q_e$  versus  $C_e$ , the  $q_{max}$  and  $K_L$  are calculated from the slope and intercept, respectively.

$$\frac{C_e}{q_e} = \frac{1}{K_L q_{max}} + \left(\frac{1}{q_{max}}\right) C_e \quad (7)$$

The Freundlich isotherm equation is expressed in Eq. (8) and the equilibrium adsorption capacity is expressed by  $q_e$  (mg/g) [43].  $C_e$  refers to the concentration of free dye ions in solution at equilibrium (mg/L). The Freundlich constant associated with adsorption capacity is expressed as  $K_F$  (mg/g). By making a graph of  $\log q_e$  versus  $\log C_e$ , the values of  $n$  and  $K_F$  are evaluated with the slope and intercept.  $1/n$  refers to a heterogeneity factor that indicates the intensity of dye adsorption on  $Fe_3O_4$ -AP. The value of  $n$  indicates the preferred adsorption process and is in the  $0.1 < 1/n < 1$  [44,45].

$$\log q_e = \log K_F + \left(\frac{1}{n}\right) \log C_e \quad (8)$$

The Temkin isotherm model is expressed in Eq. (9). Similar to

the kinetic model of Langmuir and Freundlich,  $q_e$  (mg/g) and  $C_e$  (mg/L) refer to the equilibrium adsorption capacity and the concentration of free dye ions in solution at equilibrium, respectively.  $B$  corresponds to the heat of adsorption, and  $k_T$  is the binding constant of the Temkin isotherm at equilibrium and is associated with the maximum binding energy. The relationship between  $B$  and the adsorption potential of the adsorbent is expressed in Eq. (10), where  $R$  is the universal gas constant (8.314 J/kmol);  $T$  is the temperature (K), and  $1/b_T$  (mol/J) is the adsorption potential of the adsorbent.

$$q_e = B \ln k_T + B \ln C_e \quad (9)$$

$$B = \frac{RT}{b_T} \quad (10)$$

The Temkin isotherm model was studied to determine the adsorbent-adsorbate interaction. This model assumes that the heat adsorption of all molecules in the layer decreased linearly with surface coverage. In addition, the adsorption energy, when the adsorption site was filled, decreased linearly. Likewise, the binding energy distribution was uniform up to the maximum value. By making a graph of  $q_e$  versus  $\ln C_e$ , the values of  $B$  and  $K_T$  were determined by slope and intercept values.

Based on Fig. 14 and Table 3, Freundlich and Temkin adsorption isotherms well fitted the data for MB and CR adsorption isotherms on  $Fe_3O_4$ -AP with values of  $R^2 > 0.9$ . However, the Freundlich

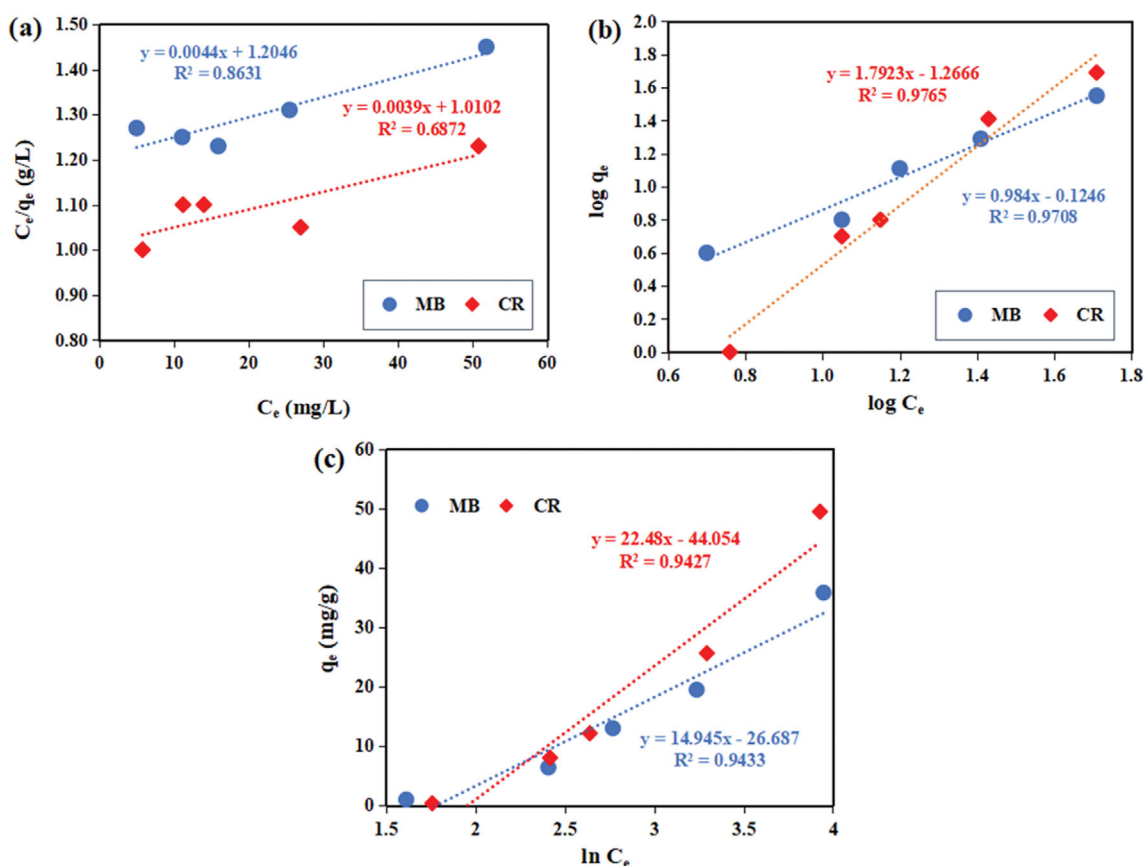


Fig. 14. (a). Langmuir, (b) Freundlich, and (c) Temkin isotherm models of MB and CR adsorption onto  $Fe_3O_4$ -AP.

**Table 3. Isotherm parameters of MB and CR dyes**

Isotherm models	Parameters	Dyes	
		MB	CR
Langmuir	$q_{max}$ (mg g <sup>-1</sup> )	227.27	256.41
	$K_L$ (L mg <sup>-1</sup> )	0.0037	0.0039
	$E_{ads}$ (kJ mg <sup>-1</sup> )	-14,044.86	-13,906.29
	$R^2$	<b>0.8631</b>	<b>0.6872</b>
Freundlich	$K_F$ (mg g <sup>-1</sup> )	16.02	10.24
	$n$	1.016	0.558
	$R^2$	<b>0.9708</b>	<b>0.9765</b>
Temkin	$B$	14.95	22.48
	$k_T$ (L mg <sup>-1</sup> )	0.17	0.14
	$1/b_T$	0.0060	0.0091
	$R^2$	<b>0.9443</b>	<b>0.9427</b>

adsorption isotherm was found to better perform with the higher values of the  $R^2$ . Freundlich isotherm model showed that various active sites played an important role in the adsorption process and had different adsorption energies but with the same entropy [43]. This finding aligned with the adsorption kinetics studies that followed Ho's second-order kinetic model. Based on Eq. (7), it was also observed that the value of  $1/n$  for MB adsorption (0.98) was smaller than 1 compared to the value for CR adsorption (1.80), indicating that the intensity of MB dye adsorption on Fe<sub>3</sub>O<sub>4</sub>-AP was

more favorable.

In addition, the value of  $1/n$  below 1 indicates that the adsorption operation was physical instead of chemical (for the value of  $1/n$  higher than 1) [44]. This also strengthened the alleged MB adsorption mechanism on Fe<sub>3</sub>O<sub>4</sub>-AP as described previously through physical adsorption. On the other hand, the preferred CR adsorption on Fe<sub>3</sub>O<sub>4</sub>-AP was chemical, while the FTIR characterization of the post-adsorption adsorbent did not show the formation of new adsorption due to chemical interactions. It became the reason that the  $K_F$  value of MB adsorption on Fe<sub>3</sub>O<sub>4</sub>-AP was higher than the  $K_F$  value of CR adsorption on Fe<sub>3</sub>O<sub>4</sub>-AP.

On the other hand, for the Temkin isotherm model ( $R^2 > 0.9$ ), the heat of adsorption of all molecules in the aqueous solution of MB and CR dyes decreased linearly with the range. The adsorbent-adsorbate interaction and adsorption were characterized by the regular allocation of binding energy until it reached the maximum binding energy [46]. Based on the  $1/b_T$  value, which showed the potential of the adsorbent, the adsorbent Fe<sub>3</sub>O<sub>4</sub>-AP had a better CR adsorption potential than MB. However, the binding constant value of the Temkin isotherm was obtained at equilibrium and was associated with a lower maximum binding energy ( $k_T$ ) for CR adsorption compared to MB.

#### 5. Performance of Fe<sub>3</sub>O<sub>4</sub>-AP as MB and CR Adsorbent

Table 4 presents the previously reported adsorption studies of various adsorbents for MB and CR removal compared with the results of this study. Compared with the results of other studies related to the adsorption of MB and CR dyes, Fe<sub>3</sub>O<sub>4</sub>-AP had an

**Table 4. MB and CR adsorption studies**

Adsorbate	Adsorbent	% Removal	Kinetic model	Fitted isotherm model	References
MB	Porous activated Starbons® derived from starch	82.6%	Pseudo-second-order and Elovich	Freundlich isotherm	[47]
MB	Orange and lemon peels-derived activated carbon (OLPAC)	98.0%	Pseudo-second-order model	Langmuir isotherms	[26]
MB	Activated carbon of Coriandrum sativum	95.0%	Pseudo-second-order kinetic	Temkin	[27]
MB	Magnetite nanoparticles using Archidendron pauciflorum peel extract (conventional)	91.7%	Pseudo-second-order kinetic	Freundlich isotherm	[19]
MB	Magnetite using Archidendron pauciflorum peel extract (sonochemical)	97%	Pseudo-second-order kinetic	Freundlich isotherm	This research
CR	MgAl-layered double hydroxide (MgAl-LDH)	14.8-100%	Pseudo-second-order kinetic	Langmuir isotherms	[40]
CR	Magnetic nanocellulose base polymeric ionic liquid	91-100%	-	Langmuir isotherms	[48]
CR	Magnetite-nanoparticle-decorated NiFe LDH (MNP@NiFe LDH)	96%	Pseudo-second-order kinetic	Langmuir isotherms	[49]
CR	Magnetite using Archidendron pauciflorum peel extract (sonochemical)	91%	Pseudo-second-order kinetic	Freundlich isotherm	This research

excellent adsorption ability even though it was synthesized using plant waste extracts. Another advantage is that adsorbents were found to be more environmentally friendly, whereas extraction solvents used was water with lower production costs. Thus,  $\text{Fe}_3\text{O}_4$ -AP has the potential to be developed as an adsorbent for MB and CR dyes.

## CONCLUSIONS

$\text{Fe}_3\text{O}_4$ -AP synthesized using the sonochemical method has great potential as an adsorbent for methylene blue and Congo red dyes in simulated wastewater.  $\text{Fe}_3\text{O}_4$ -AP synthesized using sonochemistry has high crystallinity, crystal size, and smaller particles compared to conventional methods, and other plant extracts studied previously. Also, the  $\text{Fe}_3\text{O}_4$ -AP adsorbent has superparamagnetic properties with a saturation magnetization value of 27.71 emu/g. The adsorption of MB and CR on  $\text{Fe}_3\text{O}_4$ -AP follows a pseudo-second-order Ho kinetic model with  $q_e$  values of 1,666.67 and 1,250.00 mg/g, respectively, and  $k$  values of 0.00514 and 0.00107 g/mg.min, respectively. The MB and CR adsorption isotherms on  $\text{Fe}_3\text{O}_4$ -AP follow the Freundlich isotherm model with KF values of 16.02 and 10.24 mg/g, respectively.  $\text{Fe}_3\text{O}_4$ -AP was found to be capable of absorbing MB dye better than CR dye.

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## REFERENCES

1. F. M. Valadi, A. Ekramipooya and M. R. Gholami, *J. Mol. Liq.*, **318**, 114051 (2020).
2. Q. Wei, Y. Zhang, K. Zhang, J. I. Mwasiagi, X. Zhao, C. W. K. Chow and R. Tang, *Korean J. Chem. Eng.*, **39**, 1850 (2022).
3. Y. Zheng, X. Sun, X. Liu, X. Xia, L. Xiao, C. Cao, Q. Qian and Q. Chen, *Ind. Crops Prod.*, **171**, 113930 (2021).
4. T. K. N. Tran, V. T. Le, T. H. Nguyen, V. D. Doan, Y. Vasseghian and H. S. Le, *Korean J. Chem. Eng.*, **40**, 1650 (2023).
5. H. S. Devi, M. A. Boda, M. A. Shah, S. Parveen and A. H. Wani, *Green Process. Synth.*, **8**, 38 (2019).
6. M. Mabrouk, R. M. A. El-Wahab, H. H. Beherei, M. M. Selim and D. Das, *Int. J. Pharm.*, **587**, 119658 (2020).
7. E. Guo, G. Chen, D. Yu, Y. Qiu, S. Li and Y. Yu, *J. Environ. Chem. Eng.*, **10**, 108618 (2022).
8. N. S. El-Gendy and H. N. Nassar, *Sci. Total Environ.*, **774**, 145610 (2021).
9. K. Lakshmi and R. Rangasamy, *J. Mol. Struct.*, **1224**, 129081 (2021).
10. M. Rahmayanti, I. Nurhikmah and F. Larasati, *Mol. Biol. (Mosc.)*, **16**, 68 (2021).
11. W. Liu, H. Bai, W. Gao, Z. Chen, Z. Liu, Z. Chen and J. Chen, *Korean J. Chem. Eng.*, **39**, 2792 (2022).
12. A. Sebastian, A. Nangia and M. N. V. Prasad, *J. Hazard. Mater.*, **371**, 261 (2019).
13. S. Fakhari, M. Jamzad and H. Kabiri Fard, *Green Chem. Lett. Rev.*, **12**, 19 (2019).
14. F. Azadi, A. Karimi-Jashni and M. M. Zerafat, *Ecotoxicol. Environ. Saf.*, **165**, 467 (2018).
15. C. V. Khedkar, N. D. Khupse, B. R. Thombare, P. R. Dusane, G. Lole, R. S. Devan, A. S. Deshpande and S. I. Patil, *Chem. Phys. Lett.*, **742**, 137131 (2020).
16. A. Sebastian, A. Nangia and M. N. V. Prasad, *J. Cleaner Prod.*, **174**, 355 (2018).
17. L. Hiremath, N. K. Sura and P. Sukanya, *Mater. Today Proc.*, **5**, 21030 (2018).
18. H. Luo, S. Zhang, X. Li, X. Liu, Q. Xu, J. Liu and Z. Wang, *J. Taiwan Inst. Chem. Eng.*, **72**, 163 (2017).
19. M. Rahmayanti, A. Nurul Syakina, I. Fatimah and T. Sulistyaningsih, *Chem. Phys. Lett.*, **803**, 139834 (2022).
20. S. Charungchitrak, A. Petsom, P. Sangvanich and A. Karnchanat, *Food Chem.*, **126**, 1025 (2011).
21. M. Rahmayanti, S. J. Santosa and S. Sutarno, *Adv. Mater. Res.*, **1101**, 286 (2015).
22. H. Zheng, D. Liu, Y. Zheng, S. Liang and Z. Liu, *J. Hazard. Mater.*, **167**, 141 (2009).
23. J. Wang and X. Guo, *J. Hazard. Mater.*, **390**, 122156 (2020).
24. Y. P. Yew, K. Shameli, M. Miyake, N. Kuwano, N. B. Bt Ahmad Khairudin, S. E. Bt Mohamad and K. X. Lee, *Nanoscale Res. Lett.*, **11**, 276 (2016).
25. H. Rasoulzadeh, A. Mohseni-Bandpei, M. Hosseini and M. Safari, *Int. J. Biol. Macromol.*, **133**, 712 (2019).
26. D. Ramutshatsha-Makhwedzha, A. Mavhungu, M. L. Moropeng and R. Mbaya, *Heliyon*, **8**, e09930 (2022).
27. C. C. de Souza, L. Z. M. de Souza, M. Yilmaz, M. A. de Oliveira, A. C. da Silva Bezerra, E. F. da Silva, M. R. Dumont and A. R. T. Machado, *Clean. Mater.*, **3**, 100052 (2022).
28. P. C. Nnaji, V. C. Anadebe, I. G. Ezemagu and O. D. Onukwuli, *Arab. J. Chem.*, **15**, 103629 (2022).
29. M. Rahmayanti, A. Yahdiyani and I. Q. Afifah, *Commun. Sci. Technol.*, **7**, 119 (2022).
30. L. Ouma and A. Ofomaja, *RSC Adv.*, **10**, 2812 (2020).
31. M. Rahmayanti, S. J. Santosa and S. Sutarno, *Indones. J. Chem.*, **16**, 329 (2016).
32. S. V. Bhosale, S. R. Suryawanshi, S. V. Bhoraskar, M. A. More, D. S. Joag and V. L. Mathe, *Mater. Res. Express*, **2**, 095001 (2015).
33. S. Nigam, K. C. Barick and D. Bahadur, *J. Magn. Magn. Mater.*, **323**, 237 (2011).
34. M. Masuku, L. Ouma and A. Pholosi, *Environ. Nanotechnol. Monit. Manag.*, **15**, 100429 (2021).
35. T. Babacan, D. Doğan, Ü. Erdem and A. Ü. Metin, *Mater. Chem. Phys.*, **284**, 126032 (2022).
36. M. Shamsipur and A. Ghavidast, *J. Mol. Struct.*, **1263**, 133130 (2022).
37. B. S. Damasceno, A. F. V. da Silva and A. C. V. de Araújo, *J. Environ. Chem. Eng.*, **8**, 103994 (2020).
38. R. Foroutan, R. Mohammadi and B. Ramavandi, *Environ. Sci. Pol.*

- lut. Res.*, **26**, 19523 (2019).
39. C. González-Galán, A. Luna-Triguero, J.M. Vicent-Luna, A.P. Zaderenko, A. Ślawek, R. Sánchez-de-Armas and S. Calero, *Chem. Eng. J.*, **398**, 125678 (2020).
40. M. A. Farghali, A. M. Selim, H. F. Khater, N. Bagato, W. Alharbi, K. H. Alharbi and I. Taha Radwan, *Arab. J. Chem.*, **15**, 104171 (2022).
41. L. Largitte and R. Pasquier, *Chem. Eng. Res. Des.*, **109**, 495 (2016).
42. M. Benjelloun, Y. Miyah, G. Akdemir Evrendilek, F. Zerrouq and S. Lairini, *Arab. J. Chem.*, **14**, 103031 (2021).
43. H. Freundlich, *Z. Phys. Chem.*, **57U**, 385 (1907).
44. J. Bensalah, A. Habsaoui, O. Dagdag, A. Lebdiri, I. Ismi, E. H. Rifi, I. Warad and A. Zarrouk, *Chem. Data Collect.*, **35**, 100756 (2021).
45. J. Xie, T. Yamaguchi and J.-M. Oh, *J. Solid State Chem.*, **293**, 121758 (2021).
46. M. Temkin and V. Pyzhev, *Acta Physicochim. URSS*, **12**, 327 (1940).
47. H. Li, V. L. Budarin, J. H. Clark, M. North and X. Wu, *J. Hazard. Mater.*, **436**, 129174 (2022).
48. M. H. Beyki, M. Bayat and F. Shemirani, *Bioresour. Technol.*, **218**, 326 (2016).
49. T. Taher, R. Putra, N. Rahayu Palapa and A. Lesbani, *Chem. Phys. Lett.*, **777**, 138712 (2021).
50. A. N. Syakina and M. Rahmayanti, *Chem. Data Collect.*, **44**, 101003 (2023).